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# Metal-organic Framework-mediated Nitrogen-doped Carbon for CO<sub>2</sub> Electrochemical Reduction

*Riming Wang,<sup>‡<sup>a</sup></sup> Xiaohui Sun,<sup>‡<sup>a</sup></sup> Samy Ould-Chikh,<sup>b</sup> Dmitrii Osadchii,<sup>a</sup> Fan Bai,<sup>a</sup> Freek Kapteijn,<sup>a</sup> and Jorge Gascon<sup>\*<sup>a,b</sup></sup>*

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**ABSTRACT:** A Nitrogen-doped carbon was synthesized through the pyrolysis of the well-known metal-organic framework ZIF-8, followed by a subsequent acid treatment, and has been applied as catalyst in the electrochemical reduction of carbon dioxide. The resulting electrode shows Faradaic efficiencies to carbon monoxide as high as ~78%, with hydrogen being the only by-product. Pyrolysis temperature determines the amount and the accessibility of N species in the carbon electrode, in which pyridinic-N and quaternary-N species play key roles in the selective formation of carbon monoxide.

**KEYWORDS:** Nitrogen-doped carbon, electrocatalyst, ZIF-8, MOF-mediated synthesis, CO<sub>2</sub> electrochemical reduction

## 1. INTRODUCTION

CO<sub>2</sub> concentration in the atmosphere has increased drastically since the first industrial revolution. The current CO<sub>2</sub> level is considered to have caused severe environmental problems,<sup>1</sup> increasing the need to find solutions both to revert CO<sub>2</sub> emissions and to utilize the CO<sub>2</sub> already present in the atmosphere. In both cases, valorization of CO<sub>2</sub> (as opposite to disposal or storage) may provide human kind with new routes for the production of important chemical commodities traditionally manufactured from oil. Several pathways have been proposed to utilize CO<sub>2</sub>,<sup>2</sup> such as CO<sub>2</sub> methanation,<sup>3-8</sup> reverse water gas shift,<sup>9-13</sup> CO<sub>2</sub> hydrogenation to hydrocarbons or alcohols,<sup>14-20</sup> CO<sub>2</sub> electrochemical reduction,<sup>21-26</sup> and CO<sub>2</sub> photocatalytic reduction,<sup>27</sup> *etc.* Among the above-mentioned CO<sub>2</sub> utilization methods, the electrochemical reduction of CO<sub>2</sub> seems to hold great promise in a more than likely future scenario with affordable green electricity at moderate prices. In such a scenario, it is highly desirable to selectively produce one single product, while the integration of CO<sub>2</sub> reduction products with existing chemo-catalytic technologies would be ideal. In this sense, the selective production of carbon monoxide is regarded as one of the most promising alternatives, CO being a very valuable intermediate in chemical synthesis.

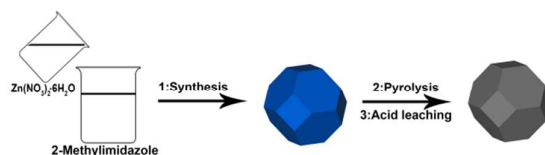
Various electrocatalysts, including noble and earth-abundant metals and their coordination complexes, have been widely studied in CO<sub>2</sub> electroreduction reaction.<sup>28-29</sup> Copper is found to be active in direct synthesis of hydrocarbons and oxygenates from CO<sub>2</sub>.<sup>30</sup> Silver and gold electrodes are reported to selectively convert CO<sub>2</sub> to CO.<sup>31-32</sup> Nevertheless, their limited availability and proneness to poisoning to a large extent impede the practical applications. Hence, the exploration of alternative materials with high energy efficiency, selectivity, and durability remains challenging.

Recently, introduction of heteroatoms (*e.g.* N, S, P *etc.*) into the carbon structure has been reported to improve the chemical, electrical, and functional properties of carbon materials.<sup>33</sup>

1  
2  
3 For instance, a carbon nanotubes (CNTs) with N as dopant show a high efficiency in CO<sub>2</sub>  
4 reduction to CO, while the nitrogen-free CNTs only produce very little amount of CO. The  
5 high CO selectivity was later attributed to the presence of pyridinic-N and quaternary-N.<sup>34-35</sup>  
6  
7 Zhang *et al.* also investigated the effect of N content in the N-doped CNTs on the catalytic  
8 activity in this reaction, and found an linear increase of the Faradaic efficiency toward  
9 formate with the N content.<sup>36</sup>

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15 Metal-organic-frameworks (MOFs) have been shown to be excellent catalyst precursors.<sup>37-</sup>  
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<sup>41</sup> The controlled thermal decomposition of MOFs in an inert atmosphere is a facile synthesis method to produce carbon materials with well-developed porosity.<sup>42-43</sup> In this study, a prototypical MOF, ZIF-8 with a nitrogen-rich organic linker, was chosen as a sacrificial template for the synthesis of N-doped carbon catalysts (NC-T, T referring the pyrolysis temperature). The synthesis involves high-temperature pyrolysis and a subsequent acid treatment (Scheme 1). The as-synthesized N-doped carbon samples were then used for CO<sub>2</sub> electrochemical reduction.



**Scheme 1.** Schematic illustration of the route to synthesize the NC-T catalysts. (1) Room temperature synthesis of ZIF-8 crystals. (2) Pyrolysis of the ZIF-8 crystals in N<sub>2</sub> at different temperatures. (3) Acid leaching to generate the NC-T catalysts.

## 2. EXPERIMENTAL SECTION

**2.1. Materials.** 2-Methylimidazole (MeIm, purity 99%), zinc nitrate hexahydrate (Zn(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, >98%), zinc acetate dihydrate (Zn(OAc)<sub>2</sub>·2H<sub>2</sub>O, >98%) and methanol

(>99.8%) were purchased from Sigma-Aldrich Chemical Co. All the chemicals were used without further purification.

**2.2. Characterization techniques.** X-ray diffraction (XRD) measurements were conducted on a Bruker D8 Advance X-ray diffractometer equipped with a Co- $K\alpha$  radiation source ( $\lambda = 0.179026$  nm). Raman spectra were obtained with a commercial Renishaw in Via Reflex confocal microscope using a 532 nm laser, and measurements were performed without any pre-treatment of samples at ambient conditions. Thermogravimetric (TG) analyses were collected using a Mettler Toledo TGA/SDTA851e instrument. The experiments were carried out from 25 °C to 1000 °C with a ramp of 5 °C·min<sup>-1</sup> under a N<sub>2</sub> flow (100 mL·min<sup>-1</sup>). The N<sub>2</sub> adsorption-desorption isotherms were measured with a Micromeritics Tristar 3020 apparatus at 77 K. Scanning electron microscopy (SEM) analysis and the EDX element mapping were performed on a Nova Nano 630 scanning electron microscope manufactured by FEI Company. Transmission electron microscopy (TEM) analysis was carried out using a FEI Titan 80-300 ST transmission electron microscope operated at 300 kV. XPS spectra were measured on a K-alpha Thermo Fisher Scientific spectrometer using monochromatic Al- $K\alpha$  radiation at room temperature and pressure inside the analysis chamber of about 10<sup>-8</sup> mbar. The obtained spectra were calibrated by setting the main peak of carbon (*C1s*) line to the reference value of  $E_b = 284.8$  eV. Thermo Advantage software package was applied for spectra processing and analysis. The spectra were deconvoluted using a mixed Gauss-Lorentz function (20% Lorentzian contribution for *C1s*, *N1s*, and *O1s*, 30% for *Zn2p*). Scofield sensitivity factors were used for the quantitative analysis. TPP-2M method was applied to eliminate the difference in analysis depth for different photoelectron lines.

### 2.3. Catalysts synthesis

*2.3.1. Synthesis of ZIF-8.* ZIF-8 precursors were synthesized according to a previously reported method with some modification.<sup>44</sup> Typically, the metal precursor and organic linker

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3 solutions were prepared by separately dissolving 2.933 g zinc nitrate hexahydrate and 6.489 g  
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5 2-methylimidazole into 200 mL methanol and kept under stirring for 15 min. The clear linker  
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7 solution was then rapidly mixed with the metal precursor solution and kept under magnetic  
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9 stirring at room temperature for 24 h. Afterwards, the bright white product was collected by  
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11 filtration, washed three times with methanol, and dried at 80 °C under vacuum.

12  
13 *2.3.2. Synthesis of MOF-5.* MOF-5 precursors were synthesized based on the previously  
14  
15 reported method with some modification.<sup>45</sup> In a typical synthesis, 5.065 g terephthalic acid  
16  
17 and 16.99 g zinc acetate dihydrate were dissolved in 400 mL and 500 mL DMF, respectively.  
18  
19 After stirring for 15 min, the zinc acetate solution was added to the organic linker solution,  
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21 and the mixture was stirred for another 2.5 h. The product was filtered and washed three times  
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23 with DMF. The final product was dried at 80 °C under vacuum.

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25 *2.3.3. Synthesis of NC-T and C-900.* For the preparation of NC-T, 1g ZIF-8 was pyrolyzed in  
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27 a ceramic crucible inside a tubular quartz reactor (approximately 1.0 m in length and 5.0 cm  
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29 in diameter) horizontally placed in a ceramic fiber oven (Carbolite, Sheffield). Nitrogen was  
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31 kept flushing through the reactor at a rate of 100 ml·min<sup>-1</sup> under 30 °C for 0.5 h,, followed by  
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33 further carbonization at different temperature for 4 h under the same N<sub>2</sub> flow. The set  
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35 temperature was reached at a ramp of 2 °C·min<sup>-1</sup>. The obtained black powders were further  
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37 immersed in 400 mL 0.5 M H<sub>2</sub>SO<sub>4</sub> solution for 24 h at 80 °C and then dried at 60 °C in a  
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39 vacuum oven for 24 h. These samples are denoted as 'NC-T', where T refers to the pyrolysis  
40  
41 temperature (T = 700, 800, 900 °C). For the synthesis of C-900, 1 g MOF-5 was pyrolyzed at  
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43 900 °C, washed in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution, and dried under vacuum at the same conditions as  
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45 that of NC-900.

## 50 **2.4. Electrochemical performance**

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52 *2.4.1. Preparation of working electrode.* For preparation of the electrode, 50 mg catalyst was  
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54 weighed and suspended in a mixture of tetrahydrofuran (4 mL), Nafion solution (0.5 mL) and  
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3 isopropyl alcohol (4 mL). Then the mixture was kept in an ultrasonic bath for 2 h. The  
4 suspension was dropcasted onto a carbon cloth electrode with an area of 12.5 cm<sup>2</sup> (2.5 cm ×  
5 2.5 cm, both sides effective). The electrode was then dried overnight at 80 °C under vacuum.  
6  
7 The final catalyst loading of ~50 mg was confirmed by weighing the working electrode before  
8 and after dropcasting process, so the catalyst per area was ~4 mg/cm<sup>2</sup>.  
9

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13 *2.4.2. CO<sub>2</sub> electrochemical reduction performance.* CO<sub>2</sub> electroreduction experiments were  
14 performed in a continuous flow reactor as previously reported. The reactor was divided into  
15 two compartments, the anode and cathode compartment, by a proton-exchange membrane.  
16 The anode compartment contained a counter electrode (Pt gauze), while the cathode electrode  
17 contained the working electrode and a reference electrode (Ag/AgCl electrode). Both  
18 compartments had a volume of 100 mL, and were filled with 85 mL electrolyte prior to the  
19 performance tests, leaving a headspace of 15 mL. CO<sub>2</sub> was then fed into the reactor by  
20 bubbling through the liquid with a flow rate of 100 mL·min<sup>-1</sup> until the electrolyte was  
21 saturated, after which the CO<sub>2</sub> flow was fixed at 10 ml·min<sup>-1</sup>. To start the controlled potential  
22 electrolysis, an operation potential was applied by a potentiostat (Autolab PGSTAT302N) in  
23 the range of -1.0 to -2.0 V vs Ag/AgCl. The cathode compartment was connected to an on-  
24 line gas chromatograph (Global Analyzer Solution Compact GC), and the on-line GC would  
25 be triggered every 24 min to analyze the gas product. All the experiments last 120 min. At the  
26 end of the electrocatalytic test, a liquid sample (~1 mL) was collected from the electrolyte  
27 solution for ultra-performance liquid chromatography (UPLC) measurement. After each  
28 experiment, the electrochemical reactor was cleaned with distilled water, and the proton-  
29 exchange membrane was immersed into 0.1 M H<sub>2</sub>SO<sub>4</sub> for regeneration.  
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50 Faradaic efficiency (FE) of the gas product was calculated based on the following equation:

$$51 \quad FE = \frac{\eta \times F \times v \times f}{V_m \times j} \quad (1)$$

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56 Where:

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3  $n$ : the number of electrons consumed to produce one product molecule, for the product of  
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5 CO or H<sub>2</sub> ( $n=2$ ), while for the product of CH<sub>4</sub> ( $n=8$ );

6  
7  $v$ : the volume fraction of a certain gas product;

8  
9  $f$ : the overall gas flow rate (in the unit of m<sup>3</sup>s<sup>-1</sup>);

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11  $F$ : Faraday constant ( $F=96485\text{ C}\cdot\text{mol}^{-1}$ );

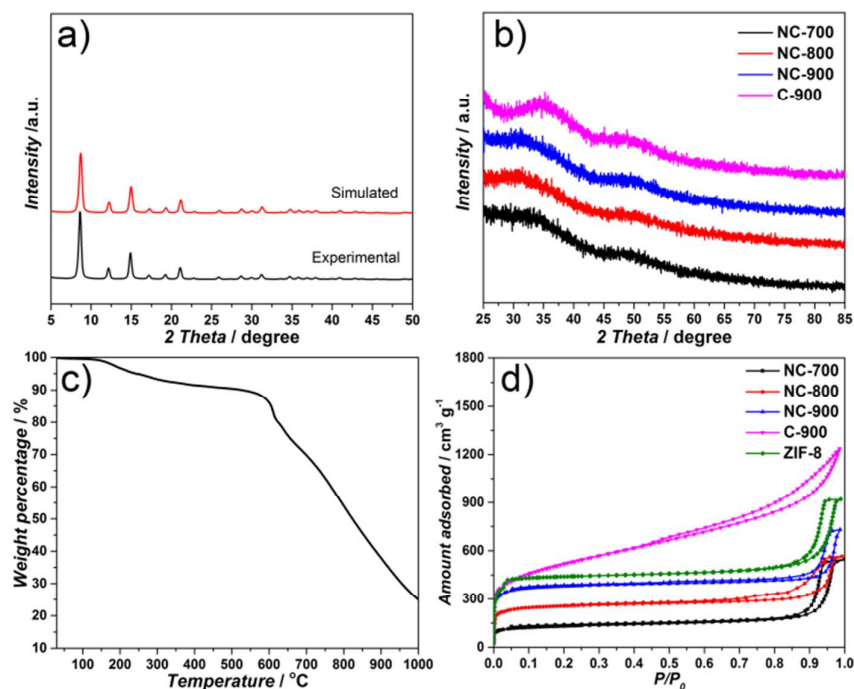
12  
13  $V_m$ : the molar volume constant at ambient pressure ( $V_m=0.024465\text{ m}^3\text{mol}^{-1}$ );

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16  $j$ : steady-state cell current at each applied potential (in the unit of A).  
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### 20 3. RESULTS AND DISCUSSION

#### 21 3.1. Synthesis and Structural Characterization.

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24 ZIF-8 was synthesized by mixing methanolic solutions of zinc nitrate and MeIm (2-  
25 methylimidazole) at room temperature.<sup>44</sup> The powder X-ray diffraction (PXRD) pattern  
26 confirms the formation of pure crystalline ZIF-8 (Figure 1a).<sup>46</sup> After pyrolysis and a  
27 subsequent acid treatment, the characteristic peaks of ZIF-8 disappear, and two broad  
28 reflections positioned at  $2\theta = 30^\circ$  and  $50.5^\circ$  are observed in the N-doped carbon samples  
29 (Figure 1b), attributed to the (002) and (100) planes of the graphitic carbon, respectively.<sup>40,47</sup>  
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**Figure 1.** XRD pattern of ZIF-8 (a) and carbon based samples (b); TG curve of ZIF-8 (c); N<sub>2</sub> sorption isotherms of the as-synthesized materials (d).

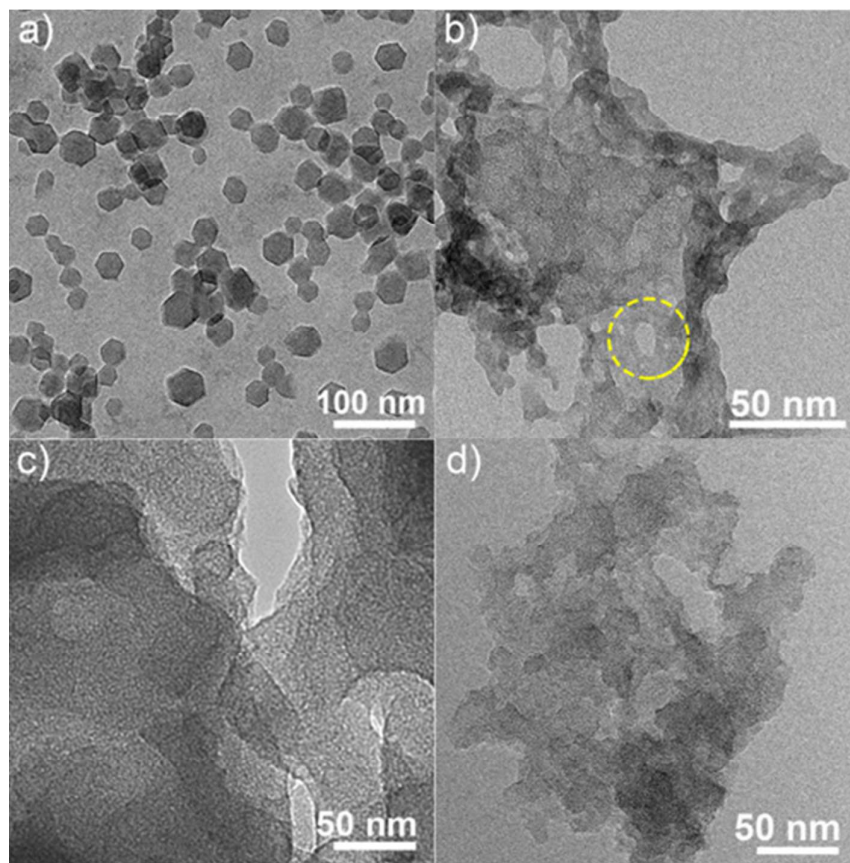
The graphitization degree of the carbon matrix in the N-doped carbon samples was analyzed by Raman spectroscopy (Figure S1). All the Raman spectra of NC-T exhibit the characteristic G and D bands of carbon at 1580 cm<sup>-1</sup> and 1350 cm<sup>-1</sup>, which are correlated to graphitic *sp*<sup>2</sup> carbon and disordered or defect carbon, respectively.<sup>39</sup> The Raman spectra exhibit an apparent correlation with pyrolysis temperature. The intensity ratio between G and D band ( $I_G/I_D$ ) is similar between NC-800 and NC-900, suggesting a comparable graphitization degree of the carbon matrix.<sup>48-49</sup> For the Raman spectrum of NC-700, a shoulder at 1500 cm<sup>-1</sup> can also be observed. This peak is likely to originate from the non-pyrolyzed imidazoles,<sup>50</sup> and leads to an overestimation of the  $I_G/I_D$  ratio. Indeed, the presence of non-pyrolyzed imidazoles in NC-700 can be further confirmed by thermogravimetric (TG) analysis (Figure 1c). In the TGA curve, a mass loss of ~ 10 wt.% can be observed until 600 °C, probably attributed to the release of moisture and residual MeIm molecules from the porosity of ZIF-8.<sup>46</sup> The sample mass then decreases sharply with elevating temperature, which can be ascribed to the

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3 decomposition of the organic linker (MeIm) and the gradual evaporation of metallic zinc  
4 (boiling point of metallic Zn: 907 °C).<sup>51-52</sup>  
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7 The Brunauer-Emmett-Teller (BET) area ( $S_{BET}$ ) and pore volume ( $V_{pore}$ ) of ZIF-8 and NC-T  
8 samples were determined by N<sub>2</sub> adsorption-desorption isotherms at 77 K (Figure 1d), and the  
9 corresponding textural properties are summarized in Table S1. ZIF-8 with a high  $S_{BET}$  of 1752  
10 m<sup>2</sup>g<sup>-1</sup> and  $V_{pore}$  of 1.42 cm<sup>3</sup>g<sup>-1</sup>, exhibits a typical microporous structure with some  
11 intergranular mesoporosity, as concluded from the presence of hysteresis loop above  $P/P_0 \approx$   
12 0.8.<sup>53</sup> After pyrolysis and acid leaching, the  $S_{BET}$  and  $V_{pore}$  of NC-T samples decrease  
13 drastically, attributed to the collapse of the well-defined microporous structure of ZIF-8  
14 during the pyrolysis process. Besides, an apparent dependence between surface area and pore  
15 volume with pyrolysis temperature can be observed in NC-T samples. Specifically, NC-900  
16 sample exhibits the highest  $S_{BET}$  and micropore volume ( $V_{micro}$ ), but the lowest mesopore  
17 volume ( $V_{meso}$ ) among all NC-T samples, suggesting that a higher pyrolysis temperature can  
18 remove more organic residuals from the pores but lead to more agglomeration of carbon  
19 nanoparticles.<sup>49</sup>  
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35 The morphology of the synthesized materials was studied using electron microscopy.  
36 Transmission electron microscopy (TEM) image (Figure 2a) of the as-prepared ZIF-8 exhibits  
37 a typical rhombic dodecahedral shape with a size of 30-50 nm. The corresponding energy-  
38 dispersive X-ray spectroscopy (EDX) element mapping images (Figure S2a-d) demonstrate  
39 the homogeneous dispersion of carbon, nitrogen, and zinc throughout the ZIF-8 crystal. After  
40 high-temperature pyrolysis and acid treatment, highly dispersed C, N, and Zn EDX-signals in  
41 the pyrolyzed NC-T samples can be detected (Figure S2e-p). The absence of any observable  
42 zinc (oxide) nanoparticles in the carbon matrix of the as-synthesized NC-T samples are  
43 further verified by TEM analysis (Figure 2b-d), indicating that the acid treatment is sufficient  
44 to remove all zinc (oxide) nanoparticles from these nitrogen-doped carbon samples. In  
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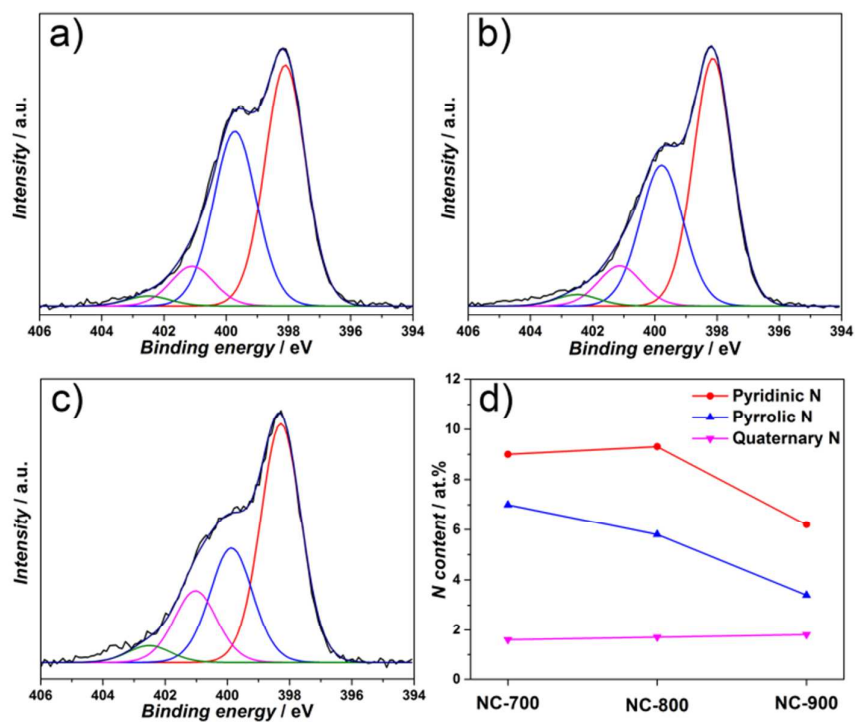
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3 addition, some large pores are observed in the NC-T samples (e.g. the yellow circle in Figure  
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5 2b), attributed to the presence of voids between nanoparticles, in line with the N<sub>2</sub> sorption  
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7 results.  
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36  
37 **Figure 2.** TEM images of ZIF-8 (a), NC-700 (b), NC-800 (c), and NC-900 (d).  
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39  
40 The as synthesized precursors and catalysts were further characterized by means of X-ray  
41 photoelectron spectroscopy (XPS). The XPS survey spectra clearly demonstrate the presence  
42 of C, N, O, and some Zn in the structure of all the samples (Figure S3 a,b and Table S2). XPS  
43 survey spectra indicate that these NC-T samples exhibit similar oxygen and zinc contents, and  
44 the presence of the *O1s* signal can be attributed to the oxidation of the carbon surface after  
45 exposure to the air together with the subsequent acid leaching. The similar Zn contents of NC-  
46 T samples detected by XPS analysis further confirm that the acid leaching easily removes  
47 those Zn (oxide) nanoparticles in the carbon porosity, while the remaining Zn signals in all  
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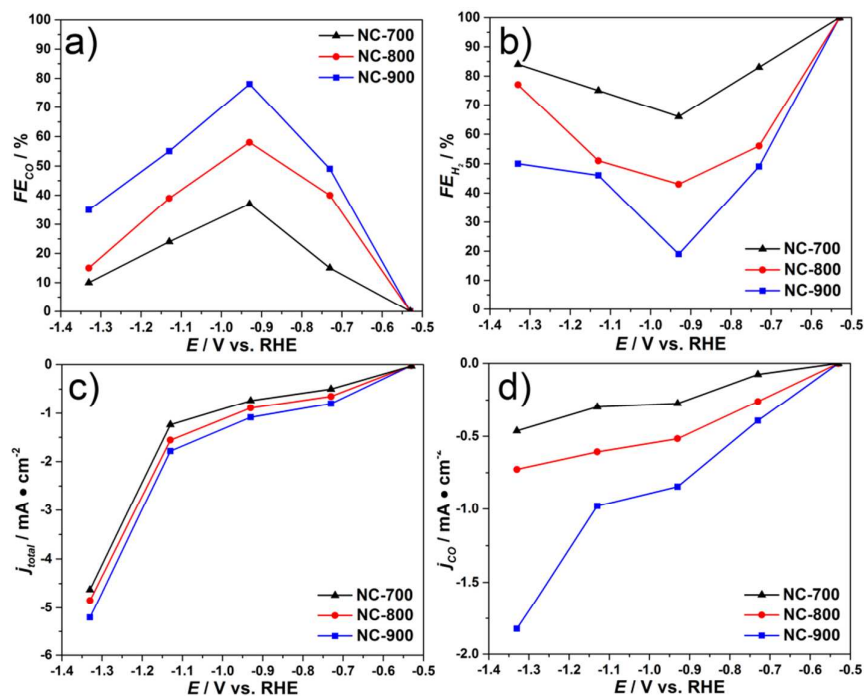
these NC-T samples have been proven by Wang *et al.* to be porphyrin-like Zn ( $\text{Zn-N}_x$ ) with high resistance against acid leaching.<sup>54</sup>  $\text{N}1s$  signals of NC-T samples can be deconvoluted into four types of nitrogen species with binding energy around 398.3 eV, 399.9 eV, 401.2 eV, and 402.5 eV, which can be attributed to pyridinic-N, pyrrolic-N, quaternary-N, and oxidized-N, respectively,<sup>55</sup> as shown in Figure 3a-c. We speculate that, upon pyrolysis, N atoms in the pentagonal ring of the original imidazole units are mostly converted into pyridinic-, pyrrolic-, and quaternary-N species. The percentage of each N species is calculated from XPS analysis and included in Figure 3d and Table S2. Obviously, the NC-T sample synthesized at a higher pyrolysis temperature contains a lower overall N content, which can be attributed to the removal of some relatively unstable N species such as pyridinic and/or pyrrolic-N at high temperature, consistent with previous reports.<sup>55-56</sup> Pyridinic-N dominates in all NC-T samples, and the NC-800 sample has the highest pyridinic-N content of 9.3 %.



**Figure 3.**  $\text{N}1s$  XPS region spectra of (a) NC-700, (b) NC-800, and (c) NC-900; (d) N species distribution in NC-900.

### 3.2. Catalysis

The performance of the N-doped carbon catalysts in the electrocatalytic reduction of carbon dioxide was evaluated in 0.1 M  $\text{KHCO}_3$  solution saturated with  $\text{CO}_2$  under controlled potential electrolysis. No liquid-phase products could be detected during the reaction by ultra-performance-liquid chromatography (UPLC), and the gas products were analyzed by an online gas chromatography (GC). As shown in Figure 4a and b, CO and  $\text{H}_2$  are the only detectable reduction products over the whole potential range, except at -1.33 V vs. RHE (reversible hydrogen electrode), where some  $\text{CH}_4$  is produced (Figure S4). When the Faradaic efficiency (FE) of CO ( $\text{FE}_{\text{CO}}$ ) is plotted as a function of the potential in the range of -0.53 to -1.33 V vs. RHE, a volcano-like curve is obtained, with an optimum at -0.93 V vs. RHE for all these N-doped carbon samples. At the same time, the  $\text{FE}_{\text{CO}}$  of NC-T samples depends on the pyrolysis temperature, and the N-doped carbon pyrolyzed at a higher temperature exhibits a higher  $\text{FE}_{\text{CO}}$ , with NC-900 showing the highest  $\text{FE}_{\text{CO}}$  of ~78% at -0.93 V vs. RHE, which is comparable to the data reported recently from nitrogen-doped carbon catalysts (Table S3).<sup>34-36,57-63</sup> The FE of  $\text{H}_2$  ( $\text{FE}_{\text{H}_2}$ ) exhibits the opposite trend to  $\text{FE}_{\text{CO}}$ , indicating that the electroreduction of  $\text{CO}_2$  reaction competes with the hydrogen evolution reaction (HER) in aqueous solutions, which can also be proven by the linear sweep voltammetry (LSV) analysis (Figure S5).<sup>58</sup> Figure 4c and d show the total current density ( $j_{\text{total}}$ ) and partial current density to CO ( $j_{\text{CO}}$ ) for the N-doped carbon samples within the potential range from -0.53 to -1.33 V vs. RHE. NC-900 exhibits the highest  $j_{\text{total}}$  and  $j_{\text{CO}}$  among these catalysts. The electrocatalytic stability of the NC-900 sample in  $\text{CO}_2$  reduction is as well evaluated by constant potential electrolysis of  $\text{CO}_2$  (Figure S6a). At an applied potential of -0.93 V vs. RHE, the NC-900 sample exhibits a stable current density of  $-1.1 \text{ mA cm}^{-2}$  and  $\text{FE}_{\text{CO}}$  of ~80% during 120 min reaction time, without obvious deactivation.



**Figure 4.** CO<sub>2</sub> electrochemical reduction performance of NC-T samples. (a) Faradaic efficiency to CO, (b) Faradaic efficiency to H<sub>2</sub>, (c) Total current density, and (d) Partial CO current density.

To probe the origin of the CO<sub>2</sub> reduction catalytic activity obtained with the NC-900 sample, a carbon material (C-900) was also prepared by pyrolysis of MOF-5 ([Zn<sub>4</sub>O(bdc)<sub>3</sub>], bdc = benzene-1,4-dicarboxylate),<sup>43</sup> followed by acid leaching under the same conditions as NC-900. As expected, C, O, and Zn signals but no N species can be detected in the XPS survey spectrum of C-900 (Figure S3 and Table S2). Although C-900 exhibits a higher  $S_{BET}$  than that of NC-900 (Figure 1d and Table S1), it shows a  $FE_{CO}$  as low as ~2%, along with a poor current density of -0.6 mA  $cm^{-2}$  at -0.93 V vs. RHE (Figure S6b). This result indicates that the presence of N in the carbon structure significantly improves the activity for CO<sub>2</sub> electroreduction. It has been reported that pyridinic-N and quaternary-N species in the carbon matrix can facilitate the transfer of a proton-electron pair to CO<sub>2</sub>, thereby lowering the energy barrier for the production of COOH\*, an intermediate for CO formation, resulting in a high catalytic activity, while the pyrrolic-N plays a less important role in this process.<sup>34-35</sup>



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3 Unexpectedly, NC-800 is less active although it has a higher total content of pyridinic-N and  
4 quaternary-N than NC-900. On one hand, zinc-porphyrin complex ( $\text{Zn-N}_x$ ) indeed was  
5 reported to preferably produce hydrogen under a similar electrochemical measurement  
6 condition,<sup>64</sup> however, since NC-900 and NC-800 exhibit similar Zn contents, as proven by  
7 XPS analysis, the lower activity of NC-800 cannot be simply attributed to the presence of  
8 these Zn species. On the other hand, NC-800 and NC-900 samples also show similar  
9 graphitization degrees according to Raman measurement. Thus, we attribute the lower activity  
10 of NC-800 mainly to the lower  $S_{BET}$  of NC-800, which probably impedes the accessibility of  
11 active sites during  $\text{CO}_2$  electroreduction process.  
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#### 24 4. CONCLUSIONS

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26 We propose a facile route for the preparation of nitrogen-doped carbon materials via  
27 pyrolysis of ZIF-8 and a subsequent acid treatment. In  $\text{CO}_2$  electroreduction, these N-doped  
28 carbon samples are up to 78% selective to CO formation, the higher pyrolysis temperature the  
29 better catalytic performance. The high activity can be attributed to the presence of a large  
30 amount of pyridinic-N and quaternary-N species in the carbon structure, which are known to  
31 lower the energy barrier for the formation of  $\text{COOH}^*$ , an intermediate to produce CO. In  
32 addition, the well-developed porosity further promotes the activity by making more active  
33 sites accessible.  
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#### 45 ASSOCIATED CONTENT

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48 **Supporting Information.** Figures of catalyst structural characterization, including Raman,  
49 SEM-EDX, XPS. Summary of  $\text{N}_2$ -physisorption and XPS data. Additional  $\text{CO}_2$   
50 electroreduction performance. This material is available free of charge via the Internet at  
51 <http://pubs.acs.org>.  
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19 **Notes**20  
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