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# Dispersion of silica-encapsulated DNA magnetic particles in a homogeneous sand tank $^{\star}$

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#### ABSTRACT

In this study, we focused on the 3D dispersion of colloids. To our knowledge, we were the first to do so. Thereto, we injected silica encapsulated DNA tagged superparamagnetic particles (SiDNAmag) in a homogeneous coarse grain sand tank. At four downstream locations, SiDNAmag concentrations were determined as a function of time. Longitudinal and transverse dispersivity values and associated uncertainties of SiDNAmag were determined using Monte Carlo modelling approach. The parameter associated uncertainties of hydraulic conductivity as well as of the effective porosity estimated from SiDNAmag breakthrough curves were statistically similar to those estimated from salt tracer breakthrough curves. Further, the SiDNAmag dispersivity uncertainty ranges were then statistically compared with the salt tracer (NaCl, and fluorescein) dispersivities. Our results indicated that time to rise, time of peak concentration and shape of the breakthrough curves of SiDNAmag were similar to those of the salt tracer breakthrough curves. Despite the size difference between the salt tracer molecules and SiD-NAmag, size exclusion did not occur, probably due to the large pore throat diameter to SiDNAmag diameter ratio. The median longitudinal dispersivity ( $\alpha_L)$  of salt tracer and SiDNAmag were 4.9 and 5.8  $\times$   $10^{-4}$  m, respectively. The median ratio of horizontal and vertical transverse dispersivities to  $\alpha_{\rm L}$ ,  $(\alpha_{\rm TH} / \alpha_{\rm L}$  and  $\alpha_{\rm TV} / \alpha_{\rm L}$ respectively), for salt tracer and SiDNAmag ranged between 0.52 and 0.56. Through the statistical tests, we concluded that the longitudinal and traverse dispersivities of SiDNAmag were not statistically significantly different from salt tracer in 3 dimensions and could be used to characterize the dispersive properties of the medium we used. Our work contributes to a better understanding of 3D dispersion of SiDNAmag in saturated porous media.

#### 1. Introduction

Estimation of longitudinal ( $\alpha_L$ ), horizontal transverse ( $\alpha_{TH}$ ), and vertical transverse dispersivities ( $\alpha_{TV}$ ) of colloids in sand is important to predict transport of colloids through sand (Chrysikopoulos and Katzourakis, 2015), and colloid associated contaminant transport (McCarthy, 2018; Won et al., 2019).

In understanding colloid transport through saturated sand, a usual approach is to consider the  $\alpha_L$  of salt tracer and colloids to be identical (Schijven et al., 2013; Tosco et al., 2012; Wang et al., 2012). Where few saturated sand column studies have observed similar arrival and time to peak for colloids as compared to conservative tracers (Solovitch et al.,

2010; Tosco et al., 2012; Wang et al., 2012), others have reported otherwise. In a number of saturated sand column studies, with a collector grain to colloid diameter ratio ranging between 100 and 110,000 [–] at average linear velocities ranging between 0.1 and 1.95 cm/min (Table 1), an earlier arrival, earlier time to peak and higher longitudinal dispersivity of colloids as compared to salt tracers, were attributed to velocity enhancement due to size exclusion of colloids and effective porosity reduction (Bennacer et al., 2013; Chrysikopoulos and Katzourakis, 2015; Chrysikopoulos and Syngouna, 2014; Grolimund et al., 1998; Higgo et al., 1993; Keller et al., 2004; Mikutis et al., 2018). A positive correlation of colloid size and longitudinal dispersivity was reported by Katzourakis and Chrysikopoulos (2021), and was attributed

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to the exclusion of larger colloids from the lower velocity regions of parabolic velocity profile of the pore throats. In micromodels, Sirivithayapakorn and Keller (2003), and James and Chrysikopoulos (2003), reported a reduction in the longitudinal dispersion coefficient and dispersivity with increasing colloid size as compared to conservative tracers. The dispersivity reduction with increasing colloid size was due to smaller colloids and the colloids migrating near the collector grain walls tended to remain near the collector grain wall without migrating to the higher velocity streamlines due to negligible diffusion, therefore, following a more tortuous path (James and Chrysikopoulos, 2003).

In addition to size exclusion and velocity enhancement, colloid retention by straining or attachment onto the collector grains could affect the longitudinal dispersivity of colloids (Vasiliadou and Chrysikopoulos, 2011; Syngouna and Chrysikopoulos, 2011) and overshadow the effect of size exclusion and velocity enhancement by colloid retardation (Grolimund et al., 1998; Keller et al., 2004; Pang et al., 2021). Attachment and remobilization of colloids resulted in an increase in the longitudinal dispersivity (de Vries et al., 2022). The minimum pore throat to colloid diameter ratio was <1.5 for size exclusion to occur (Sirivithayapakorn and Keller, 2003). In a pore network model, Meng and Yang (2019) reported that for smaller diameter particles (100 nm particle diameter as compared to 500 nm particle diameter, used by Meng and Yang (2019)), the effect of size exclusion was negligible and did not affect the longitudinal dispersivity estimation. The contrasting outcomes suggested that dispersion was not only dependent on the porous medium properties but also on the physical properties of colloids (e.g. size) and interaction with the collector grains. Because there were no trends identified between colloid dispersion behaviour and experimental physico-chemical conditions, such as, collector grain diameter, colloid diameter, average flow velocity, and pore throat to colloid diameter ratio (Table 1), a colloid (SiDNAmag) and collector grain size specific estimation of  $\alpha_L$  is required.

Horizontal transverse ( $\alpha_{TH}$ ) and vertical transverse ( $\alpha_{TV}$ ) dispersivities, in addition to  $\alpha_L$ , are also important parameters reflecting the mass transfer through the porous medium and overall concentration distribution of a plume (Bijeljic and Blunt, 2007).  $\alpha_{TV}$  and  $\alpha_{TH}$  are prevalently considered to be an order of magnitude lower than  $\alpha_L$ , which may not be true under all flow and solute transport conditions and therefore, should be determined as an independent parameter (Zech et al., 2019). The consideration of  $\alpha_{TV}$  and  $\alpha_{TH}$  being 1 order or magnitude lower than  $\alpha_L$ , was valid only for advection dominated transport (Bijeljic and Blunt, 2007). The knowledge gap that still remained unaddressed is the estimation of  $\alpha_{TV}$  and  $\alpha_{TH}$  as independent parameters, specifically for colloid transport, in a 3D system.

In order to address this knowledge gap, our objective was to estimate the  $\alpha_{\rm L}$ ,  $\alpha_{\rm TV}/\alpha_{\rm L}$ , and  $\alpha_{\rm TH}/\alpha_{\rm L}$ , of colloid, in the form of SiDNAmag, in a 3D, saturated, homogeneous and unconsolidated sand medium and evaluate the associated uncertainties of  $\alpha_{I}$ ,  $\alpha_{TV}/\alpha_{I}$ , and  $\alpha_{TH}/\alpha_{I}$ , and compare with the conservative salt tracer. Since our sand to SiDNAmag diameter is at least 1-2 order of magnitude larger than threshold of displaying size exclusion or pore clogging (Sirivithayapakorn and Keller, 2003), and small sized colloids migrate similar to conservative salt tracer (Wang et al., 2013), we hypothesize that under our experimental conditions,  $\alpha_L$ ,  $\alpha_{TV}/$   $\alpha_L$  and  $\alpha_{TH}/$   $\alpha_L$  values and associated uncertainties estimated from SiDNAmag transport would not be statistically significantly different to that of conservative tracers (null hypothesis). In order to attain the objective, we injected two uniquely sequenced SiDNAmags at two injection wells in a homogeneously packed, saturated, coarse grain sand tank. At four downstream locations, we determined the SiDNAmag concentrations as a function of time (breakthrough curves). We further estimated the longitudinal and transverse dispersivities and associated uncertainties by fitting SiDNAmag breakthrough curves through 3D advective-dispersive equation combined with first order kinetic attachment-detachment model (based on least root mean square error) using a Monte Carlo simulation approach.

DNA particles, either naked or encapsulated in polylactic acid, alginate, or silica, had been previously used for investigating subsurface flow properties, contaminant transport, and aquifer characterization in last two decades (Chakraborty et al., 2022; Foppen, 2023; Mikutis et al., 2018; Pang et al., 2020; Zhang et al., 2021). Unlike the salt or dye tracers, uniqueness in the DNA sequences imparts the advantage of DNA particles in concurrent injection experiments without background concentration interference (Chakraborty et al., 2023; Pang et al., 2020). The encapsulation provides stability to the DNA molecules against physico – chemical stressors such as pH, radiation, or enzymatic activities (Pang et al., 2020; Sharma et al., 2012). The additional advantages of DNA particles were high specificity of detection, and low detection limit in polymerase chain reaction (Dahlke et al., 2015; Foppen et al., 2011).

#### 2. Materials and methods

#### 2.1. SiDNAmag and injection suspension preparation

SiDNAmags are spherical colloidal particles with an iron oxide core and silica covering, impregnated with double stranded DNA (dsDNA) molecules (Sharma et al., 2021). The advantage of dsDNA is the low detection limit, high specificity in quantitative polymerase chain (qPCR), no background concentration interference and are unique in

Table 1

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Literature overview of experimental conditions and effect on longitudinal dispersivity, size exclusion and velocity of colloids.
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Colloids	Study	d <sub>c</sub> (nm)	d <sub>a</sub> (μm)	$\sim d_p/d_c^*$	$\sim d_t/d_c^*$	$V_{cons}$ (cm/	Effect on colloi	id transport	Reference	
	type					min)	α <sub>L</sub> (cm)	Size exclusion and velocity		
Silica DNA Silica Colloid Silica colloid	Column Field Column	159 107 30	200–630 600 0.5–1000	918–2890 4000 12–24,000	424–1600 2200 7–13,000	0.75 - 0.17	Increased – –	Enhanced Similar peak time Enhanced	Mikutis et al., (2018) Ryan et al., (1999) Higgo et al., (1993)	
Polystyrene beads	Column	50, 3000	350	5000, 150	2800, 50	0.1, 1	Decreased	Enhanced	Keller et al., (2004)	
Polystyrene microspheres	Column	30–5500	2000	50,000–265	27,000–148	0.5–2	Increased with increasing size	Enhanced	Chrysikopoulos and Katzourakis, (2015)	
Kaolinite, Pseudomonas putida	Column	Kaolinite <2000, <i>P. putida</i> = 2400(900)	2000	Kaolinite = 600, <i>P. putida</i> = 700	Kaolinite = 340, <i>P. putida</i> = 400	0.98–1.95	Increased	Kaolinite retarded, <i>P. putida</i> enhanced	Vasiliadou and Chrysikopoulos, (2011)	
E. coli	Column	2000 (600)	425–600	155–220	90–120	0.72	Decreased	No enhancement/ retardation	Syngouna and Chrysikopoulos, (2012)	

<sup>\*</sup> approximated from  $d_p = 0.73d_a$  and  $dt = 0.56d_p$  (correlation applicable to simple cubic packing) (Ren and Santamarina, 2018).

nucleotide sequences providing the advantage of multipoint groundwater flow tracing (Mikutis et al., 2018; Pang et al., 2020). The superparamagnetic property of the iron oxide core imparts the advantage of rapid magnetic separation, therefore, there are no sample volume and up-concentration limitations (Sharma et al., 2021).

At first, we diluted 50  $\mu$ l of stock suspensions of 0.75 mg/ml (~10<sup>10</sup> particles/ml) of two uniquely sequenced SiDNAmags (SiDNAmag<sub>1</sub> and SiDNAmag<sub>2</sub>) (Particle Engineering Research Centre, NTNU, Norway) to 5 ml (~10<sup>8</sup> particles/ml) of demineralized water. We treated the 5 ml SiDNAmag suspensions with 1  $\mu$ l of bleach to remove any free DNA. After dividing the 5 ml suspensions into 1 ml aliquots, we washed the SiDNAmags to remove any traces of bleach. We further prepared the injection suspensions by diluting the 5 ml SiDNAmag suspension into 495 ml (~10<sup>6</sup> particles/ml) of tap water (EC 550  $\mu$ S/cm; pH 7.0; hardness 145.36 mg/l). The diameter of SiDNAmag<sub>1</sub> and SiDNAmag<sub>2</sub> were 206.4  $\pm$  85.6 nm and 183.9  $\pm$  58.1 nm with a unimodal size distribution and zeta ( $\zeta$ ) potentials of -11 mV and -14 mV in demineralized water, respectively. We measured the hydrodynamic diameter (D<sub>hvd</sub>)

and the electrophoretic mobility of the SiDNAmags (at a concentration of  ${\sim}10^7$  particles/ml) in tap water using Smoluchowski's equation (Malvern Panalytical Zetasizer Nano-Zs ZEN 3600, the Netherlands). The  $D_{hvd}$  were measured using 173° dynamic light backscattering.

#### 2.2. Sand tank experiments, and sample analysis

We wet packed a 1.3 m long (1.3 m  $\times$  0.7 m  $\times$  0.4 m) PVC tank with coarse grain quartz sand (500–700 µm) to represent an unconsolidated, homogeneous aquifer system (Fig. 1). The tank dimension was determined through pre-modelling exercise using flow and solute transport module (MT3D) considering suitable transport length, effect of injection volume of flow, and interaction of injection water with tank boundaries. We ensured the homogeneity of the tank by settling the sand through repetitive saturation and desaturation with tap water. Prior to the experiments, we conducted several small scale (10–20 cm) salt transport experiments to validate the homogeneity of the sand and suspending the sand dust in tap water at a concentration of 0.01 g/ml. The sand grain size

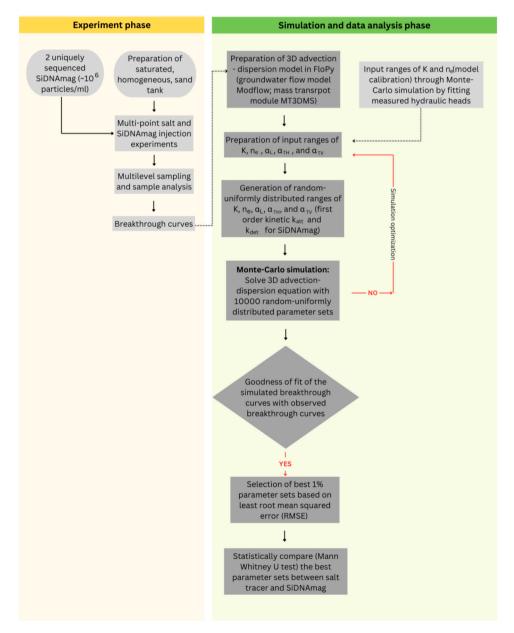


Fig. 1. Laboratory and simulation methodology flowchart.

distribution was measured by dry sieve analysis (Fritsch vibrating sieve, Dijkstra vereenigde, the Netherlands). The  $d_{60}$ ,  $d_{50}$  and  $d_{10}$  of the sand were 665, 630, and 370 µm (coefficient on uniformity =  $d_{60}/d_{10} = 1.8$ ), respectively. The bulk density of the sand was 1623 kg/m<sup>3</sup>. We estimated the pore diameter ( $d_p$ ) and pore throat diameter ( $d_t$ ) from sand grain characteristics using (Ren and Santamarina, 2018)

$$d_{p} = 8 \frac{\sqrt[7]{\frac{K}{K_{0}}} \rho_{w} G_{s} D_{50}}{3(C_{u} + 7)\rho_{m}}$$
(1a)

 $d_t = 0.56d_p \tag{1b}$ 

Where  $\gamma$  is the sensitivity of hydraulic conductivity to void ratio. We considered a value of  $\gamma = 3$ , as suggested by Ren and Santamarina (2018) for coarse gain sand. *K* is the hydraulic conductivity (m/min),  $K_0$  is the reference hydraulic conductivity at reference void ratio ( $e_0 = 1$ ),  $\rho_w$  is the density of sand (g/m<sup>3</sup>),  $G_s$  is the specific gravity of the sand,  $D_{50}$  is the media grain diameter (m), *Cu* is the coefficient of uniformity and  $\rho_m$  is the mass density of the sand (g/m<sup>3</sup>) (refer to Ren and Santamarina (2018) for more details). The estimated mean pore diameter to SiD-NAmag diameter ratio was  $\sim 1.19 \times 10^3 \pm 5.34 \times 10$  (Auset and Keller, 2004). The median pore throat diameter to SiDNAmag diameter ratio was  $\sim 6.69 \times 10^2 \pm 2.99 \times 10$  (Auset and Keller, 2004).

We installed two injection wells and one multilevel sampling well at a longitudinal distance of 0.3 m ( $Inj_1$ ), 0.6 m ( $Inj_2$ ), and 1.1 m ( $W_1$ ,  $W_2$ ,  $W_3$ ) from the inflow chamber, respectively on single flowline. The screens of the injection wells were installed at a depth of 13–16 cm from the bottom of the tank. The screens of the multilevel sampling well were installed at depths of 7–10 cm, 13–16 cm, and 19–22 cm from the bottom of the tank. Another sampling well ( $W_4$ ) was placed 3 cm – 4 cm away from the multilevel sampling well, transverse horizontally perpendicular to the flow line (Fig. 2).

At first, we conditioned the sand with flowing tap water for 14–15 h. During the experiments, tap water was constantly pumped (Masterflex 7528–30, Vernon Hills, USA) into the inflow chamber at a rate of  $511 \pm 7.1$  ml/min. Inflow ( $511 \pm 7.1$  ml/min) and outflow ( $505 \pm 7.3$  ml/min) rates (water balance discrepancy <5%) were monitored gravimetrically (SBSPF100A1, Steinberg Systems, Germany) in order to maintain a steady inflow. We monitored the hydraulic heads manually at 8 different

locations inside the sand tank and by water level data loggers at the inflow (~0.36  $\pm$  0.002 m) and outflow (~0.31  $\pm$  0.001 m) chambers (Fig. 2) (TD-Diver, Van Essen Instruments B. V., the Netherlands). Further, we injected (Dirac pulse) 100 ml of 0.017 g/l fluoresceindisodium salt (Acros Organics B.V.B.A., Thermofisher Scientific, the Netherlands) and 500 ml of 1.8 g/l of NaCl (J.T. Baker, the Netherlands) solution in Inj1 and Inj2, sequentially in order to avoid any influence of fluorescein-disodium salt on the electric conductivity, and therefore interference with the NaCl breakthrough curves. Because of the uniqueness of the DNA sequences in the SiDNAmags, we injected the different particles at the same time. The fluorescein and NaCl concentrations were analysed by measuring the absorbance at 489 nm using UV-visible spectrometer (Lambda 365, PerkinElmer, USA) and electric conductivity (Cond3310, WTW, Wiilheim, Germany), respectively. SiDNAmag concentrations were quantified by measuring DNA concentrations using quantitative polymerase chain reaction (qPCR) (Biorad, USA), as described by Chakraborty et al. (2022). The salt tracer breakthrough datapoints (Fig. 3), were background concentration subtracted as

$$\frac{EC}{EC_0} = \frac{EC - EC_{BG}}{EC_0 - EC_{BG}}$$
(2)

where EC,  $EC_0$ , and  $EC_{BG}$  [µS/cm], were observed, injected and background electric conductivity. We presented the salt and SiDNAmag breakthrough curves with only the datapoints above the background concentration and No template control (NTC), respectively.

#### 2.3. Breakthrough curve analysis and 3D modelling

We compared the characteristics of the experimental breakthrough curves (BTC) between the salt tracers and SiDNAmags in terms of time of maximum effluent concentration ( $t_{peak}$ ), maximum effluent relative concentration ( $C_{max}/C_0$ ) and time of  $C_{max}/C_0$  for all sampling locations. Then we estimated the distributions of the  $\alpha_L$ ,  $\alpha_{TV}/\alpha_L$ , and  $\alpha_{TH}/\alpha_L$  of the salt tracers and the SiDNAmags, by subjecting the BTCs to convective-diffusive transport modelling adopting a Monte Carlo approach.

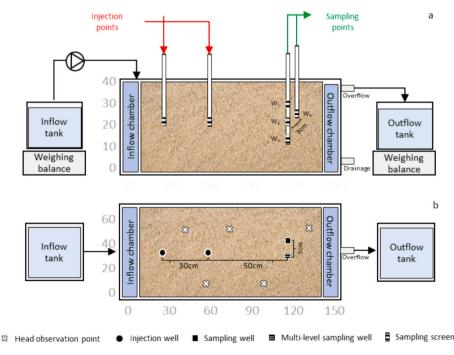
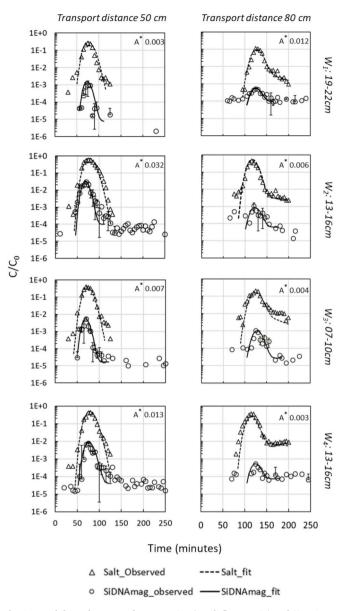


Fig. 2. Schematic experimental setup.



**Fig. 3.** Breakthrough curves of conservative (NaCl, fluorescein) and SiDNAmag for 50 cm (1a, 2a, 3a and 4a) and 80 cm (1b, 2b, 3b, 4b) transport distance at  $W_1$ ,  $W_2$ ,  $W_3$  and  $W_4$  sampling locations.

#### 2.4. Monte Carlo simulation and parameter uncertainty analysis

We estimated the  $\alpha_L$ ,  $\alpha_{TV}/\alpha_L$ , and  $\alpha_{TH}/\alpha_L$  distributions using a 3D block-centred finite difference groundwater flow model Modflow-2005 (Harbaugh et al., 2017) in combination with the mass transport module, MT3DMS (Zheng and Wang, 1999). We solved the groundwater flow (equation not shown) in conjunction with solute transport (eq. 3) equation using an iteration based generalized conjugate solver in a python package, FloPy (Bakker et al., 2016). For the simulations, we used only the observed datapoints above background concentration (for NaCl and fluorescein) and above no template control (for SiDNAmags). Thereto, we could negate the influence of the datapoints below the background concentrations on the objective function. We considered first order kinetic attachment and detachment processes were the differences between the salt tracer and the SiDNAmag transport through the saturated sand (Chakraborty et al., 2022). The mass (salt and SiD-NAmag) transport equation (Zheng and Wang, 1999) was

$$n_{e}\frac{\partial C}{\partial t} + k_{att}n_{e}C - k_{det}\rho_{b}S = \frac{\partial}{\partial x_{i}}\left(n_{e}D_{ij}\frac{\partial C}{\partial x_{j}}\right) - \frac{\partial}{\partial x_{i}}(n_{e}v_{i}C) \tag{3}$$

Where  $n_e$  is the effective porosity of the sand [-], C is the concentration of the salt tracer or SiDNAmag in the water, D<sub>ij</sub> is the hydrodynamic dispersion coefficient tensor  $[m^2/min]$ ,  $k_{att}$  and  $k_{det}$  are the first order kinetic attachment and detachment rates of the colloids [1/min],  $v_i$  is the linear pore water velocity [m/min], S is the SiDNAmag concentration at the solid surface of the sand [kg/kg],  $\rho_b$  is the bulk density of the sand  $[kg/m^3]$  and t is the time [min]. In the mass transport module for SiDNAmag transport,  $k_{att}$  is expressed as  $\beta/n_e$  [1/min] and  $k_{det}$  is expressed as  $\beta/\rho_b k_d$  [1/min], where  $\beta$  is the mass transfer rate from water to sand  $[1/\min]$  and  $k_d$  is the distribution coefficient  $[m^3/kg]$ (Babakhani, 2019). We did not consider straining to be important since the colloid to sand grain diameter ratio was well below the threshold of 0.004 (Johnson et al., 2010) or 0.003 (Bradford and Bettahar, 2006). Though fluorescein dye is conventionally used as non-reactive conservative tracer, a number of studies had demonstrated a weak sorption capacity of fluorescein onto soils (Gerke et al., 2008; Torrentó et al., 2018). Therefore, we included the attachment and detachment terms for fluorescein as well.

We discretized the 0.36 m high sand tank spatially in 12 horizontal and variably confined-unconfined layers of equal thickness considering a specified constant head boundary condition. We temporally discretized transient mass transport simulations with a Dirichlet boundary condition in three stress periods (50, 1, 300 min) for stabilizing the hydraulic head distribution, solute or SiDNAmag injection and sampling period, respectively. We estimated the input ranges of hydraulic conductivity (K) from the Darcy flux and observed hydraulic gradients in observation wells. In a homogeneous groundwater flow model, (MOD-FLOW-2005 in a python package, FloPy), we also solved groundwater flow equation, for 10,000 random-uniformly sampled parameter value sets (Monte Carlo realizations) of K and  $n_e$  to simulate the observed hydraulic heads and optimize K and  $n_e$ . Based on the maximum objective function (coefficient of determination, R (Babakhani, 2019), we considered the best 1% of the K and  $n_e$  value sets as the input ranges. The input ranges of K and  $n_e$  were 0.07–0.1 m/min and 0.2–0.4 [-], respectively. In the homogeneous flow model, combined with a 3D mass transport module (MT3DMS), we solved the mass transport equation (eq. 3) for 10,000 random - uniformly sampled parameter sets (Monte Carlo realizations) of  $\alpha_L$ ,  $\alpha_{TH} / \alpha_L$ , and  $\alpha_{TV} / \alpha_L$ . The input ranges for  $\alpha_L$ ,  $\alpha_{TV}/\alpha_L$ , and  $\alpha_{TH}/\alpha_L$  were  $10^{-6}-10^{-1}$  [m], 0.01–1, and 0.01–1, respectively for both the salt tracer and the SiDNAmag. For SiDNAmag transport simulations, we used input ranges of 0.001-0.1 [1/min] and 0.001–0.1 [m<sup>3</sup>/kg], for  $\beta$  and k<sub>d</sub>, respectively, to represent the first order kinetic attachment and detachment of SiDNAmag onto the collector sand grains. The goodness of fit of the parameter sets were evaluated based on root mean squared error (RMSE), both for individual sampling locations and combined for all sampling locations and transport distances (C-RMSE) (Ward et al., 2017). Based on the least C-RMSE, we considered the best 1% parameter sets as the parameter sets to construct the distributions of  $\alpha_L$ ,  $\alpha_{TH}/\alpha_L$ , and  $\alpha_{TV}/\alpha_L$ . We assessed the normality of the distributions using Kolmogorov - Smirnov test and Quantile -Quantile plot (QQ plot). Due to non-normality of few of the distributions, we evaluated the statistical significance of differences for each parameter, for conservative tracers and SiDNAmag using distribution non-specific Mann Whitney U test. The fitted breakthrough curves (Fig. 3) were based on the best parameter sets obtained for each parameter.

#### 3. Results

#### 3.1. SiDNAmag and sand characterization

The  $\zeta$  potential of the two SiDNAmags (at a concentration of  $\sim 10^7$ 

particles/ml) were - 22.9  $\pm$  0.05 and - 22.06  $\pm$  4.3 mV in the tap water, respectively. The  $D_{hyd}$  for the SiDNAmags were 586  $\pm$  30.7 and 688  $\pm$  69.5 nm, respectively. Under quiescent condition,  $D_{hyd}$  of the SiDNAmags, did not alter significantly throughout the experiment interval (Table 2), indicating SiDNAmag aggregation was unlikely to occur during the experiments. The  $\zeta$  potential of the quartz sand was  $-26.3\pm$ 7.9 mV, suggesting an unfavourable SiDNAmag – sand grain attachment condition.

#### 3.2. Conservative and SiDNAmag breakthrough curves

The tpeaks of the salt tracer for 0.5 m transport distance ranged between 70 and 80 min, similar to 70-75 min for SiDNAmag. At 0.8 m transport distance the  $t_{\text{peaks}}$  of the salt tracer ranged between 115 and 125 min, which was similar to the  $t_{peaks}$  of 120–125 min for the SiD-NAmag (Table 2). For both the salt tracer and SiDNAmag, we observed maximum effluent concentration at W<sub>2</sub>, as compared to W<sub>1</sub>, W<sub>3</sub> and W<sub>4</sub>, due to sampling at the same depth (0.13–0.16 m from the bottom of the tank) and flow line as the injection depth. A  $C_{\text{max}}/C_0 < 1$  for salt tracer was due to mixing through longitudinal dispersion, horizontal transverse and vertical transverse dispersion. We observed a 1-3 log reduction in C<sub>max</sub>/C<sub>0</sub> of SiDNAmag as compared to the salt tracer, and SiDNAmag to salt mass recovery ratio of 0.003-0.032, due to first order kinetic attachment in combination with  $\alpha_L$ ,  $\alpha_{TH}$ ,  $\alpha_{TV}$ , and SiDNAmag plume mixing with background water (Fig. 3). Except for the sampling location W1 for 0.5 m transport distance, all breakthrough curves had breakthrough curve tailing. The tailings were possibly due to the detachment of the SiDNAmags from sand grains. However, we did not include the complete tail datapoints in the modelling and parameter estimation process since the SiDNAmag concentrations were near no template control (NTC) and similar to the scattered datapoints prior to the breakthrough. Therefore, we treated the breakthrough tail datapoints near NTC as sample analysis uncertainty and did not include for the parameter estimation method. For fluorescein, injected at a transport distance of 0.8 m from the sampling points, we observed breakthrough tailing, possibly due to the detachment of the attached fluorescein from the sand grains (Table 2).

#### 3.3. Parameter estimation

The RMSE of the individual sampling locations for 50 cm transport distance ranged between 0.034 and 0.074 and 0.006–0.085 for the salt and SiDNAmag, respectively. For 80 cm transport distance, the RMSE of the individual sampling locations ranged between 0.029 and 0.105 and  $7.93 \times 10^{-5}$ – $2.22 \times 10^{-4}$  for salt and SiDNAmag, respectively. C-RMSE for both the transport distances and all sampling locations ranged between 0.023 and 0.025 and  $1.86 \times 10^{-3}$  -  $1.97 \times 10^{-3}$  for the salt tracer and the SiDNAmag. Based on the best 1% parameter sets estimated from objective function of RMSE for all sampling points combined, the median K values for the salt and the SiDNAmag were 0.078 and 0.082 m/min, respectively. The K value uncertainty (5th – 95th percentile) for the salt tracer and the SiDNAmag were 0.074–0.081, and 0.079–0.085 m/min, respectively. Parameter distributions of n<sub>e</sub> for all the sampling locations combined ranged between 0.29 and 0.35, and 0.27–0.35 [–], for the salt and SiDNAmag, respectively.

The median  $\alpha_L$ , for the salt and the SiDNAmag estimated from sampling locations combined were  $4.9\times10^{-4}$  and  $5.8\times10^{-4}$  m, with a 5th – 95th percentile ranges of  $6.7\times10^{-5}$ –9.1 $\times10^{-4}$ , and  $5.6\times10^{-5}$ –9.5 $\times10^{-4}$  m, respectively. The median  $\alpha_{TH}/\alpha_L$ , and the  $\alpha_{TV}/\alpha_L$  for both the salt and the SiDNAmag estimated from all sampling points combined ranged between 0.52 and 0.56 [–] with a 5th – 95th percentile of 0.09–0.94 [–]. The 5th – 95th percentile ranges for each parameter for combined simulations are summarized in Table 2. A QQ plot and Kolmogorov – Smirnov test analysis (data not shown) indicated nonnormality of the parameter distributions of the  $\alpha_L$ ,  $\alpha_{TH}/\alpha_L$ , and  $\alpha_{TV}/\alpha_L$ .

individual sampling location or from all locations combined for SiD-NAmag were not statistically significantly different from the parameter distributions estimated from salt tracer breakthrough curves, when compared using distribution non-specific Mann Whitney *U* test. The parameter distributions of k, n<sub>e</sub>,  $\alpha_{L}$ ,  $\alpha_{TV}/\alpha_{L}$ , and  $\alpha_{TH}/\alpha_{L}$ , estimated from the salt and SiDNAmag breakthrough curves, and simulations combined for all transport distances and sampling locations has been shown as box plots with 5th – 95th percentile ranges in Fig. 4. For both the salt and the SiDNAmag, the parameter values and uncertainty ranges estimated from individual sampling locations were statistically similar to the all sampling locations combined. Therefore, we presented only the ranges estimated from all sampling locations combined.

The 1–3 log reduction in the  $C_{max}/C_0$  of SiDNAmag, as compared to the conservative salt tracer was due to first order kinetic attachment of SiDNAmag onto the collector grains. The  $k_{att}$  for simulations combined for all the sampling locations and distances was 0.063 [1/min] with a 5th – 95th percentile ranges of 0.055–0.11 [1/min]. The  $k_{det}$  of the combined simulations was  $3.26 \times 10^{-4}$  [1/min] with a 5th – 95th percentile range of  $1.48 \times 10^{-4}$  to  $1.58 \times 10^{-3}$  [1/min]. The  $k_{det}$  were approximately 3 orders of magnitude lesser than that of  $k_{att}$ . The tailing of the fluorescein breakthrough curves could be explained through a low first order kinetic sorption ranging between  $8.5 \times 10^{-4} \cdot 1.9 \times 10^{-4}$  [1/min], indicating the weak sorption behaviour of fluorescein.

#### 4. Discussion

The statistically similar  $\alpha_L$ ,  $\alpha_{TH} / \alpha_L$ , and  $\alpha_{TV} / \alpha_L$  parameter distributions for both the salt tracer and the SiDNAmag indicated that SiD-NAmags had similar 3D dispersive behaviour as the salt tracer. The 1-3 log difference in maximum effluent concentration between the salt tracer and the SiDNAmags implied that a significant fraction of injected SiDNAmags could reach the sand grain surfaces, which are the low velocity regions in the parabolic Poiseuille's velocity profile in pores and pore throats, leading to colloid attachment onto the collector grains. Further, as observed by Auset and Keller (2004) in micromodel for smaller colloids (2 µm), the SiDNAmags possibly tended to remain in the low velocity streamlines and migrated along the sand grain surfaces. Therefore, SiDNAmags were not restricted to high velocity streamlines. Hence, as observed by Auset and Keller (2004) and Guo et al. (2016) for smaller particles in microscale, in our experiments the SiDNAmags probably travelled through as tortuous path as the salt tracer, resulting in similar 3D dispersive behaviour. In addition to low diffusion, the sand - SiDNAmag repulsion (charge exclusion) probably was not significant enough to force the SiDNAmags to move from grain surface (low velocity streamlines) towards the high velocity streamlines (Puls and Powell, 1992).

The SiDNAmags did not exhibit an earlier breakthrough or velocity enhancement at any of the sampling locations. This could be due to two orders of magnitude higher pore throat size as compared to the SiD-NAmag diameter. This ratio was higher than the threshold of  $d_t/d_c$  of 1.5, the ratio below which colloids cannot enter the pore (Sirivithayapakorn and Keller, 2003). However, our results were not similar to Mikutis et al. (2018), even with similar colloid size (159 nm) and sand grain size (200 - 630 µm) used in both the studies. Unlike Mikutis et al. (2018), we did not observe increased colloid velocity and increased longitudinal dispersivity. The difference could be due to lower Darcy (0.2 cm/min) and average linear velocity (0.65 cm/min) applied in our sand tank, as longitudinal dispersivity of colloids was reported to increase with increasing interstitial fluid velocity, by Chrysikopoulos and Katzourakis (2015).

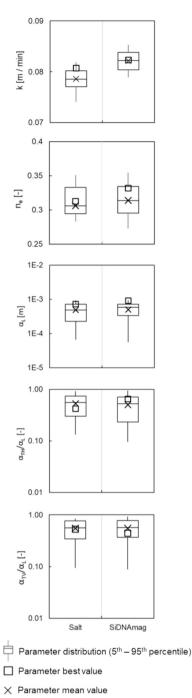
At the lowest average linear velocity (0.5 cm/min), which was similar to our study (~0.65 cm/min), Chrysikopoulos and Katzourakis (2015) did not observe velocity enhancement for any of the colloid sizes. However, the longitudinal dispersivity of colloids was higher than the conservative tracer, which could be due to the larger glass beads (2000  $\mu$ m) than the mean sand grain diameter we used (630  $\mu$ m). This is

### Table 2

 $\overline{\phantom{a}}$ 

	Transport			Tracer characteristics					cteristics	Parameter distributions						
	distance [m]		ζ - potential	D <sub>hyd</sub> [nm]			C <sub>max</sub> /C <sub>0</sub>	t <sub>peak</sub>	K [m/min]	n <sub>e</sub> [-]	α <sub>L</sub> [m]	$\alpha_{TH}  / \alpha_L$	$\alpha_{TV}  /  \alpha_L$	K <sub>att</sub>	K <sub>det</sub>	
			[mV]	0 min	0 min 60 min		240 min	[-]	[min]				[-]	[-]	[1/min]	[1/min]
Salt tracer	0.5	$W_1$					$2.5 imes 10^{-1}$	75								
		$W_2$						$5.7 imes$ $10^{-1}$	75							
		$W_3$						$5.0 imes$ $10^{-1}$	70						-	-
		$W_4$						$4.2 imes$ $10^{-1}$	80	0.078 (0.074–0.081)	0.31	$\begin{array}{l} 4.9\times 10^{-4} \\ (6.7\times 10^{-5} - \\ 9.1\times 10^{-4}) \end{array}$	0.55 (0.12 - 0.92)	0.56		
	0.8	$W_1$		-				$1.1 imes 10^{-1}$	120		(0.29–0.35)			(0.1 - 0.94)		
		$W_2$						$4.4  imes 10^{-1}$	115						$8.5 imes10^{-4}$ –1.9	$5 \times 10^{-7}$ -1.1
		$W_3$					$3.9 imes 10^{-1}$	115						$ imes 10^{-3}$	$ imes 10^{-6}$	
		$W_4$						$1.9  imes 10^{-1}$	125							
SiDNAmag	0.5	$W_1$	$22.9 \pm 0.05 \qquad \begin{array}{c} 586 \\ \pm 31 \end{array}$					$9.5 \times 10^{-4}$	70							
		$W_2$		547	525	599	$2.9 \times 10^{-2}$	70								
		$W_3$			± 41	$\pm$ 81	± 99	$5.3  imes 10^{-3}$	70							
		$W_4$						$7.7 imes$ $10^{-3}$	75	0.082	0.31	$5.8 imes10^{-4}$	0.52	0.56	0.063	$3.2 imes10^{-4}$
	0.8	$W_1$	$\begin{array}{ccc} 22.06 \pm 4.3 & \begin{array}{c} 688 \\ \pm \ 69 \end{array}$		$\begin{array}{c} 625 \\ \pm 52 \end{array}$	613	688	$5.1 imes$ $10^{-4}$	125	(0.079 - 0.085)	(0.27 0.35)	$(5.6 imes 10^{-5} - 9.5 imes 10^{-4})$	(0.09 - 0.94)	(0.09 - 0.92)	(0.05-0.1)	$(1.5 imes 10^{-4} - 1.6 imes 10^{-3})$
		$W_2$		688				$1.1 \times 10^{-2}$	120							
		$W_3$				± 89	± 79	$5.3 \times 10^{-4}$	120							
		$W_4$						$1.0 \times 10^{-4}$	125							

Salt and SiDNAmag breakthrough curves characteristics and estimated parameter distributions for hydraulic conductivity, effective porosity, longitudinal dispersivity, vertical and horizontal transverse dispersivities. The parameter ranges are presented as median (5th – 95th percentile) (K<sub>att</sub> and K<sub>det</sub> was not considered for 0.5 transport length since we assumed no sorption-desorption for NaCl tracer).



**Fig. 4.** Parameter distribution of  $\alpha_L$  [m] (a),  $\alpha_{TH} / \alpha_L$  [-] (b) and  $\alpha_{TV} / \alpha_L$  [-] (c), for conservative tracers (NaCl and Fluorescein) and SiDNAmag particles. (Box = quartiles; horizontal line = median; whiskers = 5th – 95th percentile; X

= mean of the distribution.

because smaller grain size produces less heterogeneity in the pore size distribution and more irregularity in grain shape increases continuity between medium and large pores (He et al., 2021). Heterogeneity in pore size distribution, in turn, influences the longitudinal dispersivity of colloids (Baumann et al., 2010). In addition, a linear increase in longitudinal dispersivity of colloids as compared to conservative tracer was also observed with increasing interstitial velocity (Chrysikopoulos and Katzourakis, 2015). In our work, the average linear velocity of pore water, therefore, was possibly sufficiently low to observe statistically similar longitudinal dispersivity of SiDNAmag, as compared to salt tracers. While using a 25 nm diameter silica particle, which was

approximately 9–10 times smaller than our SiDNAmag, the earlier breakthrough of silica particles, as compared to conservative tritium tracer, observed by Higgo et al. (1993) in column experiments, was possibly due to the wide grain size distribution of the column sand (0.5–1000  $\mu$ m) and therefore heterogeneity in the pore size distribution. This possibly explains why our results differ with regards to the occurrence of size exclusion observed in saturated sand columns by Higgo et al. (1993). It was not possible to reconcile the results of this study with the observations of varying extent of size exclusion, velocity enhancement and longitudinal dispersivity alteration for colloids reported by Grolimund et al. (1998); Higgo et al. (1993); James and Chrysikopoulos (2003); Keller et al. (2004) due to the differences in all the experimental conditions, such as, flow rate, average linear velocity, colloid size and porous media grain size.

In our study, the ratio of median transverse dispersivities for both the salt tracer and the SiDNAmag was higher than the oftentimes accepted value of 0.1 (Bijeljic and Blunt, 2007). This is possibly due to a low peclet number and a low average fluid velocity. Bijeljic and Blunt (2007) reported the  $\alpha_{TV} / \alpha_L$  and  $\alpha_{TH} / \alpha_L$  for solutes can be as high as ~1 at low peclet number (0.5–1) and decreased with increasing peclet number. In order to further characterize the mechanism of 3D dispersion of SiD-NAmags and compare with the salt tracer, a pore scale modelling is required (Auset and Keller, 2004; Baumann et al., 2010). However, pore scale observation was not within the scope of this study.

While our research underscored the usefulness of SiDNAmag in determining the longitudinal and transverse dispersivities of sand media, it is essential to acknowledge the limitations of this study. The universality of our finding that the longitudinal dispersivity, transverse dispersivity and associated uncertainties estimated form the salt tracer and SiDNAmag were statistically not different, is restricted. This is because the colloid transport and dispersivities in porous media, in general, is dependent on several physico-chemical experimental conditions. Dispersivities of colloidal particles depend on sand grain size (Syngouna and Chrysikopoulos, 2011), colloid diameter (Auset and Keller, 2004; Guo et al., 2016), and flow velocity (Auset and Keller, 2004). Our conclusion that dispersivities of SiDNAmag was similar to those of salt tracers apply sand grain size and colloid diameter used in this study. Transport behaviour of SiDNAmag was analysed from fitting a first order kinetic attachment – detachment model to the breakthrough curves. This approach did not allow to distinguish between colloid retention mechanisms.

#### 5. Conclusion

5.1. From the salt tracer and colloid (SiDNAmag) particle transport experiments, under our experimental conditions, we found that the longitudinal dispersivity, horizontal transverse and vertical transverse dispersivities of SiDNAmags were similar to the salt tracers. Therefore, we can accept our null hypothesis.

5.2. The parameter distributions of longitudinal dispersivity, horizontal and vertical transverse dispersivities estimated from the individual sampling locations were not statistically significantly different as compared to the distributions estimated from the simulations combined for all sampling distance and locations.

5.3. The SiDNAmags did not show size exclusion or velocity enhancement under current experimental conditions. Due to that, the longitudinal and transverse dispersivities for SiDNAmags were similar to the salt tracer.

5.4. The implication of this study lies in, as applied in our experiments, when the collector grain diameter is few orders of magnitude higher than the colloid diameter, the colloids have similar threedimensional dispersive behaviour and can be applied to predict the transport of solute tracer plumes in 3D.

5.5. However, SiDNAmag attachment onto the collector sand grains reduced the maximum effluent concentration by 1–3 orders of magnitude as compared to the conservative salt tracer, indicating a potential

limitation of SiDNAmag application in investigations involving long transport distances.

#### CRediT authorship contribution statement

**Swagatam Chakraborty:** Writing – review & editing, Writing – original draft, Visualization, Methodology, Data curation, Conceptualization. **Rayan Elhaj:** Investigation. **Jan Willem Foppen:** Writing – review & editing, Supervision, Resources, Methodology, Investigation, Conceptualization. **Jack F. Schijven:** Writing – review & editing, Supervision, Resources, Methodology, Conceptualization.

#### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Data availability

The data can be available upon request.

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